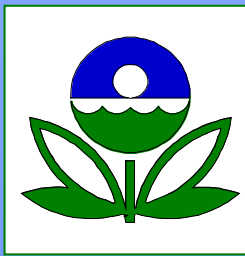




SEAR Wastewater Treatment: Contaminant Removal and Material Recovery

U.S. Environmental Protection Agency
National Risk Management Research Laboratory
Cincinnati, Ohio

SEAR Workshop



Outline

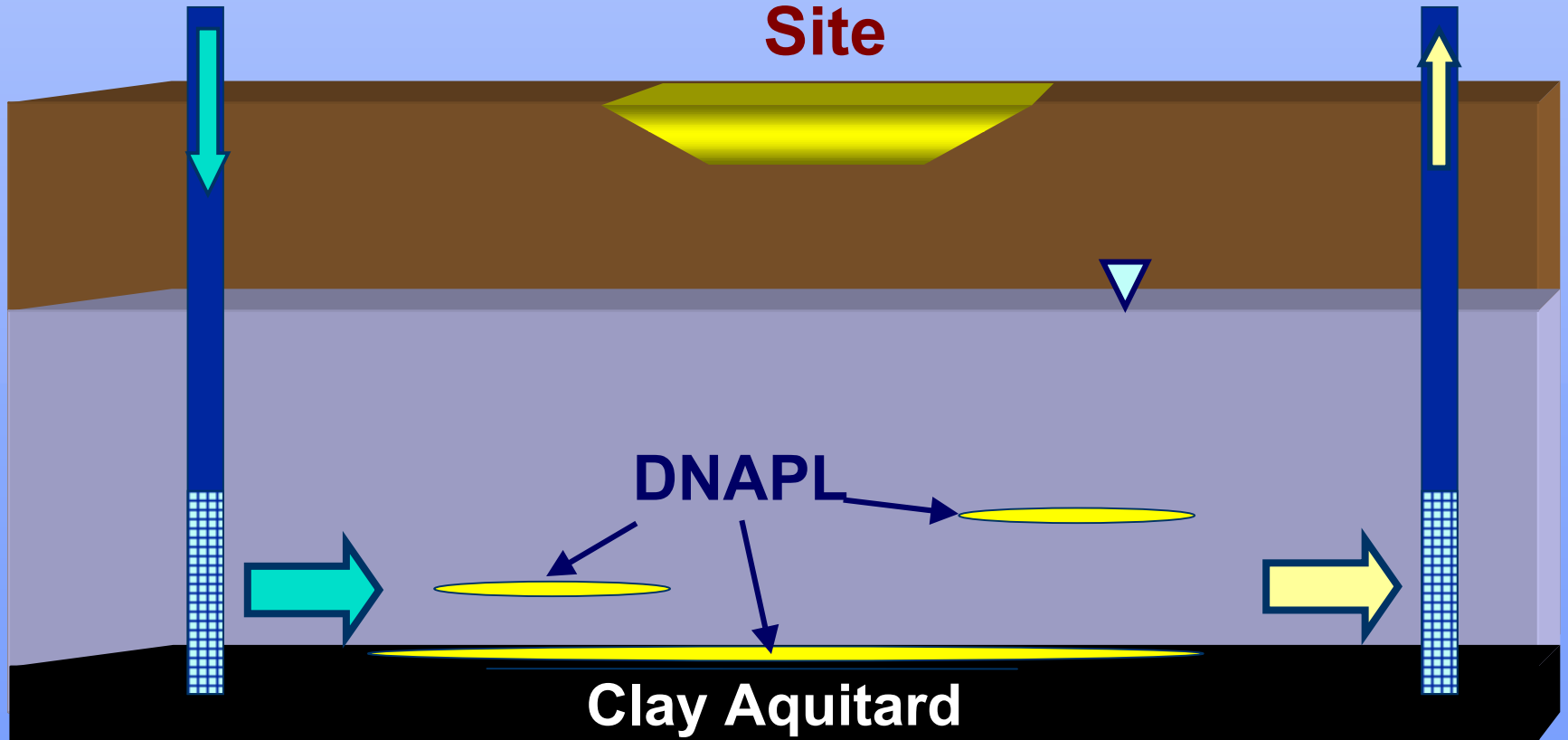
- Motivation for Treatment
- Contaminant Removal Options
- Surfactant Recovery Options
- Co-Solvent Recovery Options
- Case Study
 - ESTCP Demonstration at MCB Camp Lejeune
- Conclusions

In Situ Soil Flushing/Flooding

**Flushing Solution
Injection Well**

**Solvent
Disposal
Site**

**Extraction
Well**



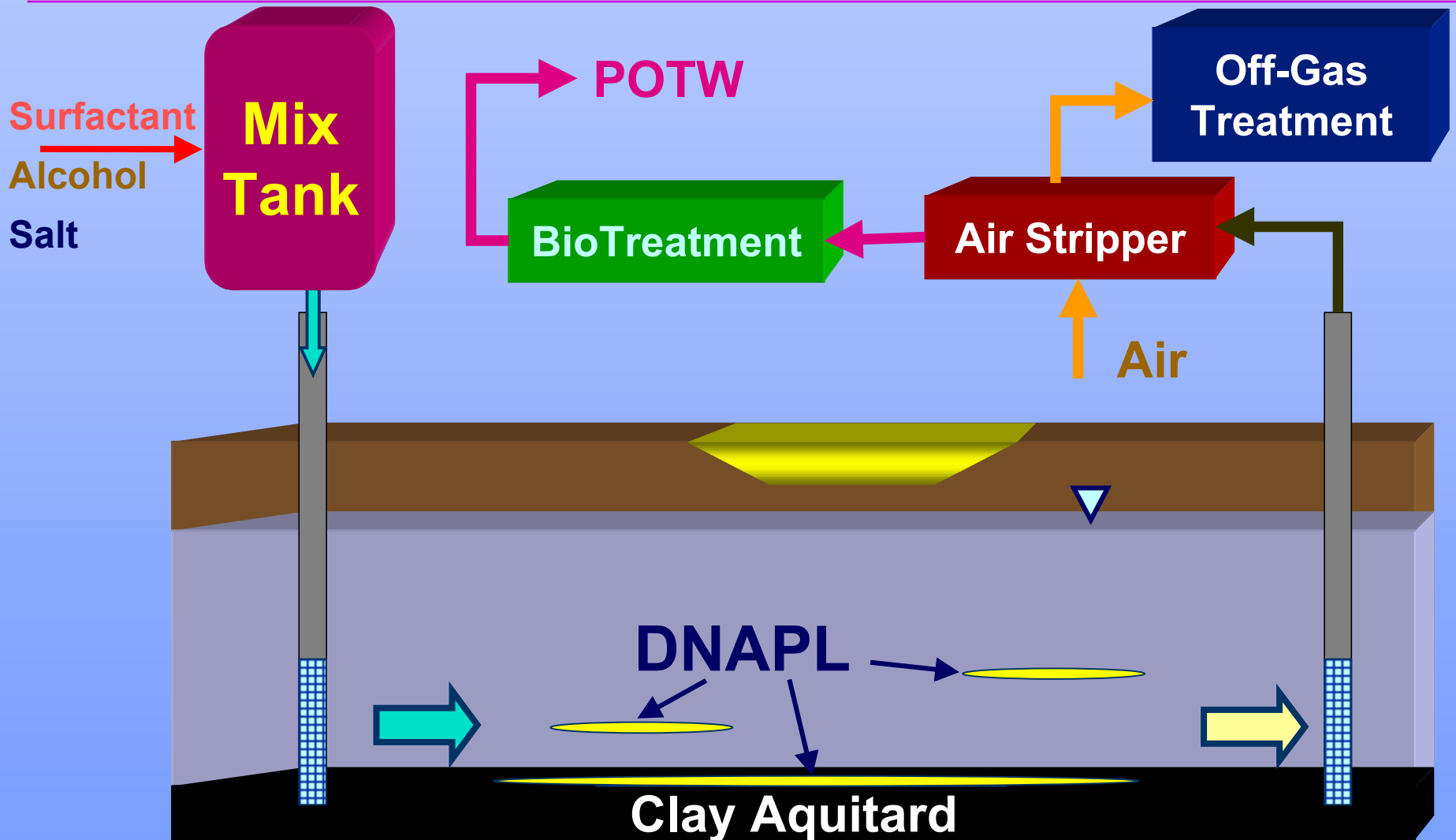
Example Properties of Extracted SEAR Fluid

- Surfactant = 0 to 6 wt%
- Alcohol = 0 to 6 wt%
- Contaminant = 0 to 10,000 mg/L
- pH = 4 to 8
- Ca^{2+} and/or Na^{+} = 0 to 250 mg/L
- Fe^{2+} = 0 to 20 mg/L
- Extraction rate > injection rate

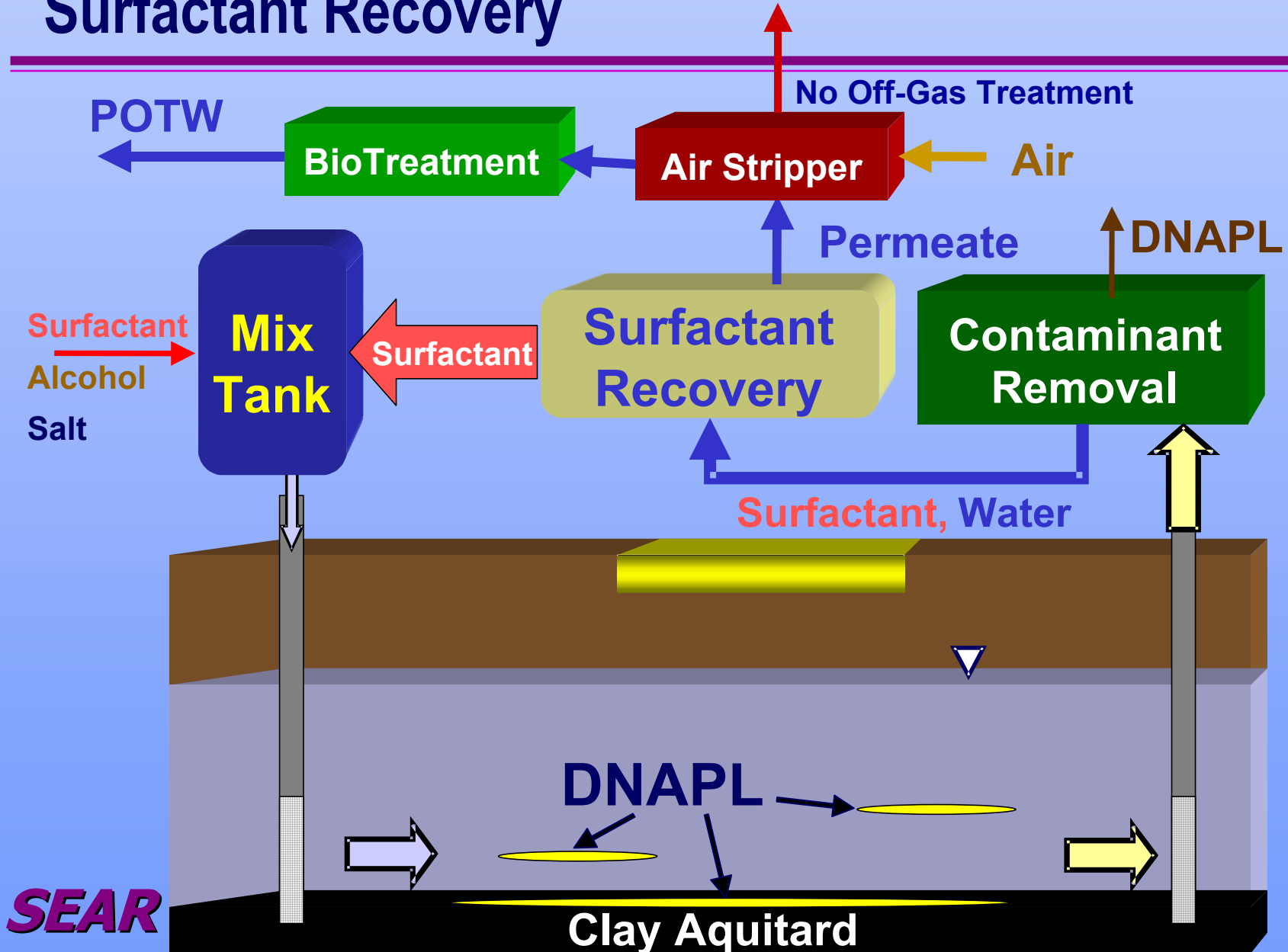
Motivations for Treatment

- Disposal Constraints at Site
 - BOD/COD
 - Hazardous compounds
 - Nuisance foam
- Desire/Requirement to Reuse Surfactant and/or Co-Solvents
 - Material savings
 - Cost savings

Basic Wastewater Treatment Without Surfactant Recovery



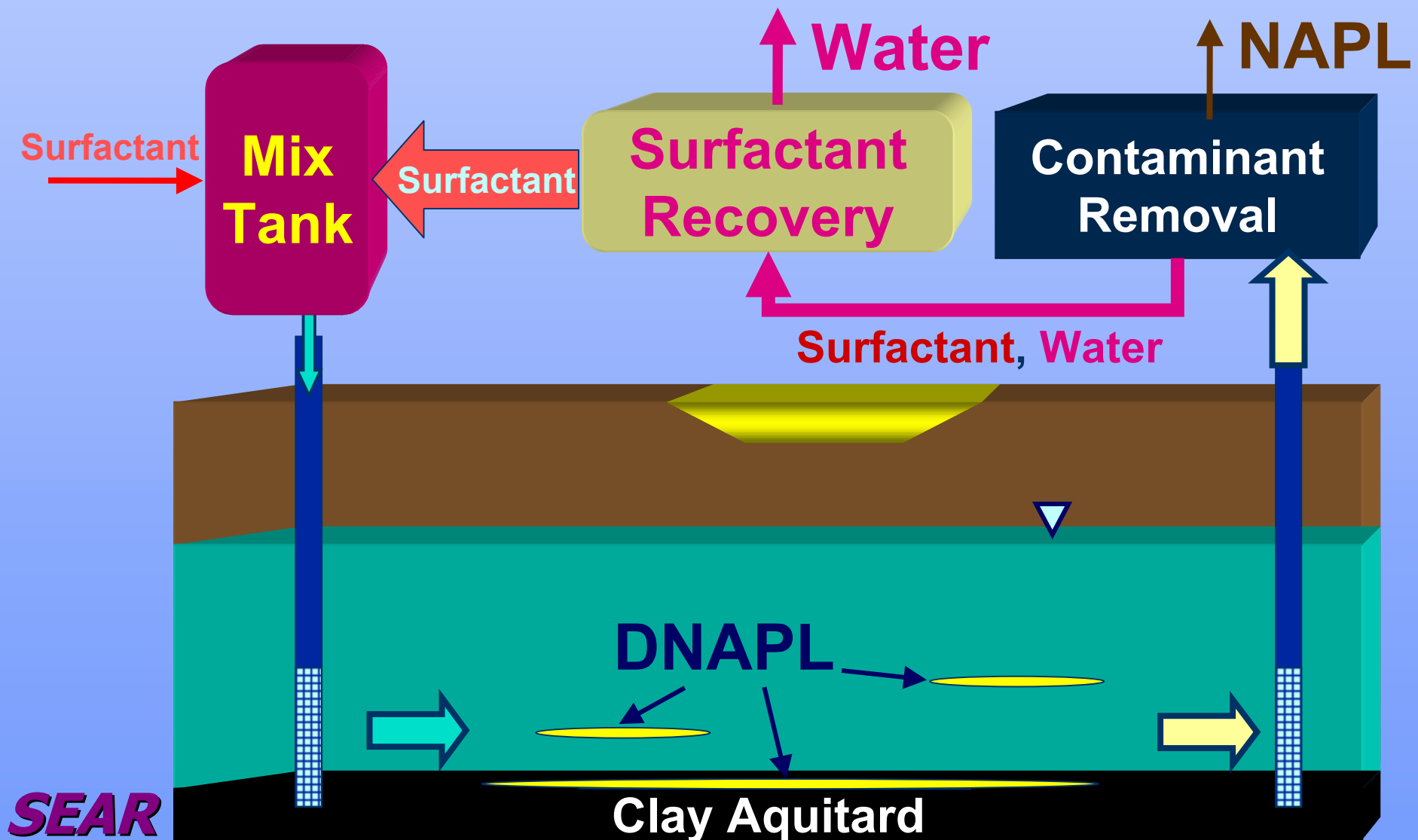
Wastewater Treatment With Surfactant Recovery



Material Recovery Example: Assumptions

- Surfactant Cost = \$5/lb-active
- Surfactant Injection Concentration = 4.0 wt%
- Surfactant Recovery Cost = \$4 per 1,000 gallons
- Contaminant Removal Cost = \$29 per 1,000 gal
- Surfactant Injection Rate = 4 gpm
- Extraction Rate = 10 gpm
- Single-Pass Recovery of Surfactant = 85%
- Single-Pass Surfactant Soil Losses = 10%

Surfactant Recovery Economics



Material and Cost Savings Spreadsheet

Contaminant Removal Expenses (\$/1000 gal)	29.00	Surf. Conc. in Extracted Fluid (wt%) =	1.44
Disposal Costs for Surfactant Solution (\$/gal)	0.50	Feed Rate of Surfactant (lb/day) =	1919.23
Surfactant Cost (\$/lb active)	5.00	Surfactant Extraction Rate (lb/day) =	1727.31
		Surfactant Recovered (lb/day) =	1468.21
Surfactant Recovery Expenses (\$/1000 gal)	4.00	Add. Surf. Needed for Reinjection (lb/day) =	451.02
Recovery of Surf. (% of feed to UF)	85		
Single Pass Soil Loss of Surf. (as % of surf. fed)	10	Material Savings =	77%
Surfactant Injection Concentration (wt%)	4.00		
Injection Flow Rate (gal/min)	4	Cost of Surfactant with recycle (\$/day) =	2255.10
		Cost of Surfactant without recycle (\$/day) =	9596.16
Extraction Flow Rate (gal/min)	10		
Density of Fluid (lb/gal)	8.33	Cost of Pervap (\$/day) =	417.60
		Cost of Ultrafiltration (\$/day) =	57.60
		Total Cost with Recycle (\$/day) =	2730.30
		Surf. Cost Without Recycle - no disposal (\$/day) =	9596.16
		Cost Savings =	71.5%
		Annual Savings (\$) =	2.51E+06
		Potential Disposal Costs for Surf. Solution (\$/day) =	7200.00

Result #1: Material Savings

Surfactant Injected = 1,900 lb/day

Surfactant Recovered = 1,500 lb/day

77% Material Recovery

Result #2: Cost Savings

- Surfactant Cost without Recycling = \$9,600/day
- Total Cost with Recycling = \$2,740/day
 - Fresh Surfactant = \$2,260/day
 - Surfactant Recovery = \$60/day
 - Contaminant Removal = \$420/day

72% Cost Savings

\$2.5 million saved per year

Disposal Cost Avoidance: Up to \$7,200/day

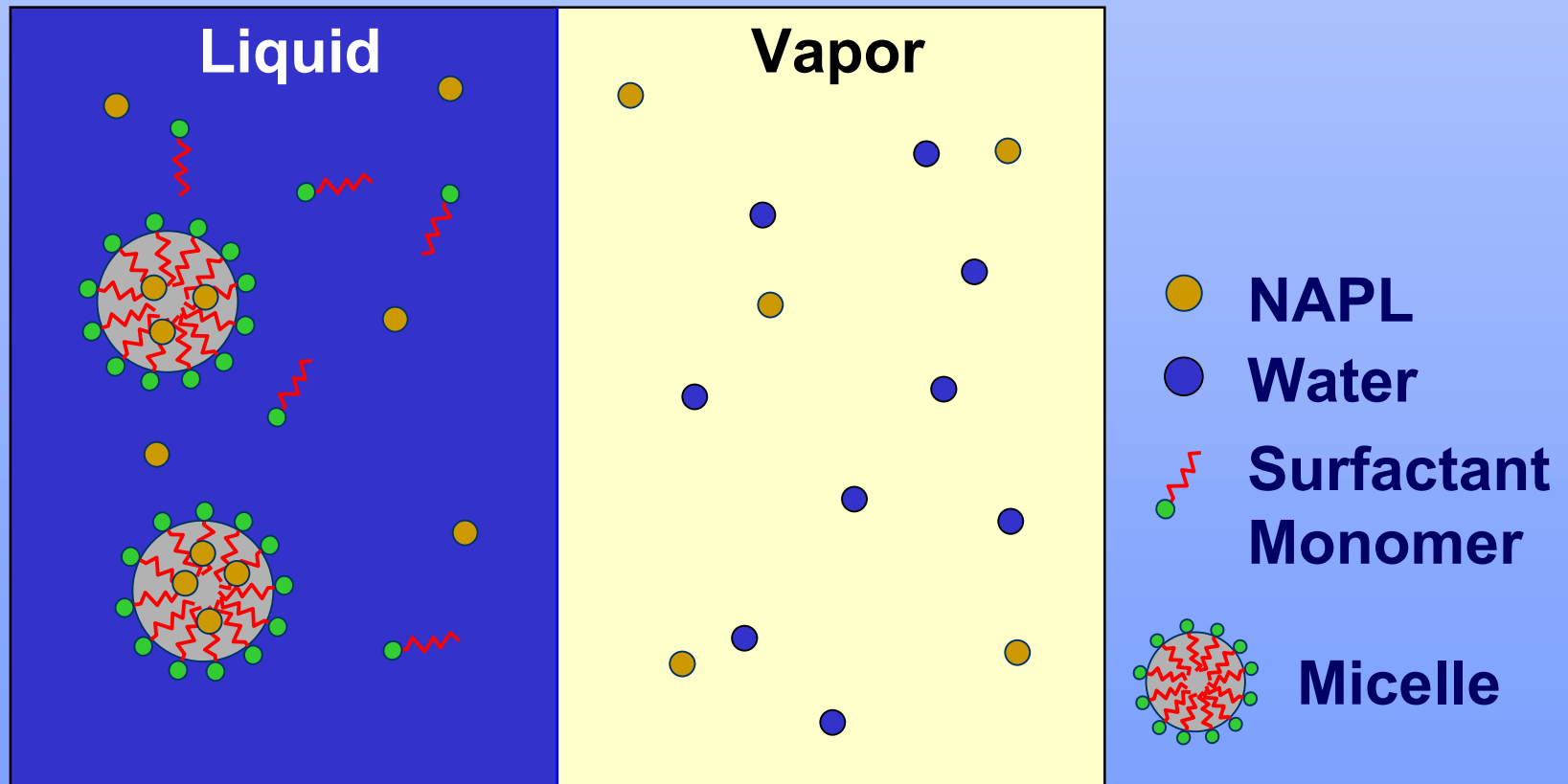
Complicating Factors

- Other streams to be treated
- Additional technologies to be operated
 - Logistics
 - Staff inexperience
 - More things to go wrong

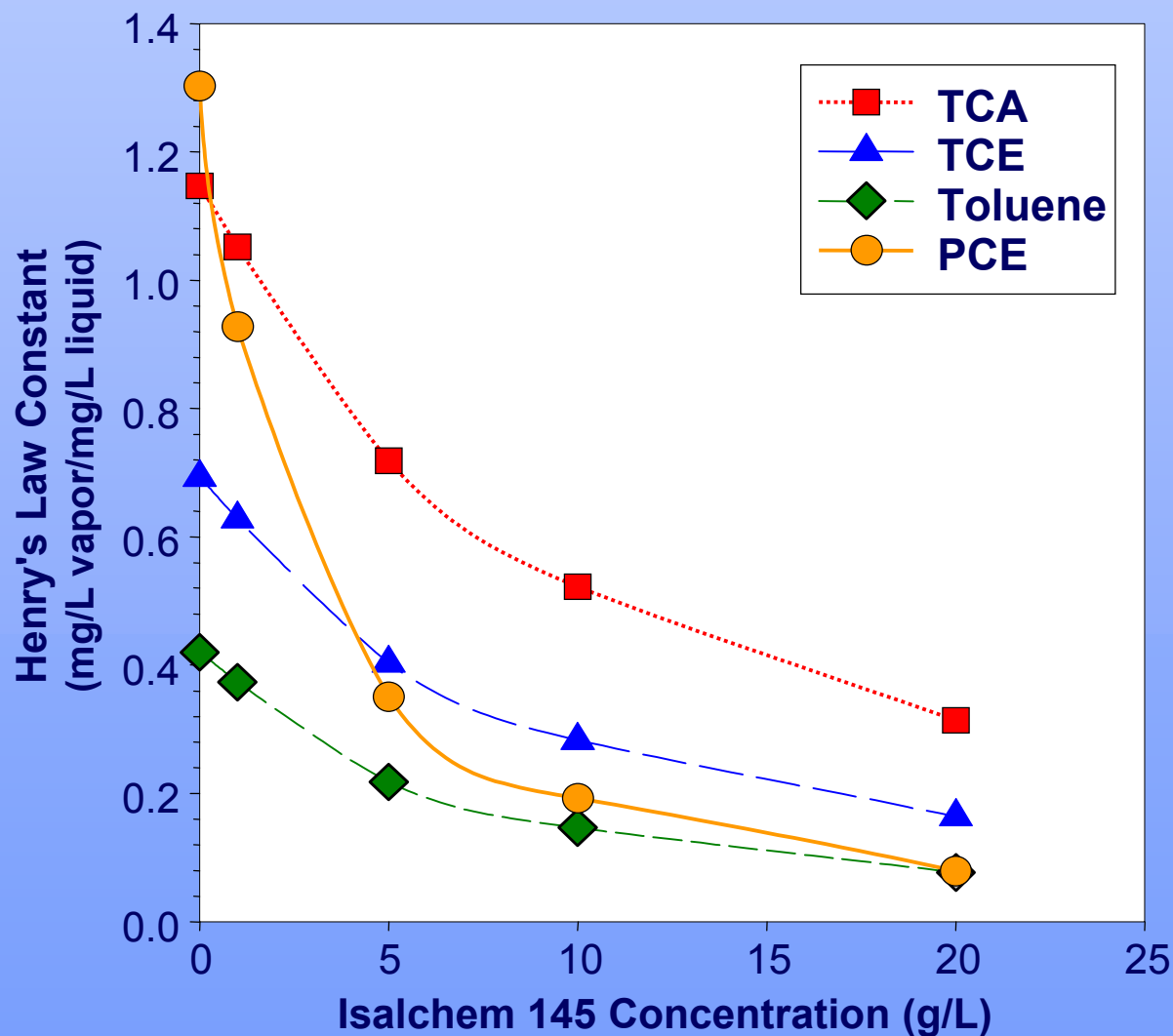
Contaminant Removal Technologies

- Air Stripping
- Steam Stripping
- Pervaporation
- Vacuum Stripping
- Catalysis/Reaction
- Distillation
- Liquid/Liquid Extraction
- Adsorption or Absorption
- Precipitation (of surfactant)

Vapor-Liquid Stripping Processes: Air, Steam, Vacuum



Surfactant Reduces Henry's Law Constant



Air Stripping

- Contaminants
 - Volatile
- Advantages
 - Low cost
 - Deep experience base
- Disadvantages
 - Foaming
 - Off-gas treatment required
 - Poor alcohol removal

Steam Stripping

- Contaminants
 - Volatile and semivolatile
- Advantages
 - Mature technology
 - Applicable to range of contaminants
- Disadvantages
 - Foaming
 - More expensive

Liquid/Liquid Extraction

- Contaminants
 - Volatile, semivolatile, non-volatile
- Advantages
 - Applicable to range of contaminants
 - No foaming
- Disadvantages
 - Stability of interface
 - Emerging technology
 - More difficult regeneration

Adsorption/Absorption

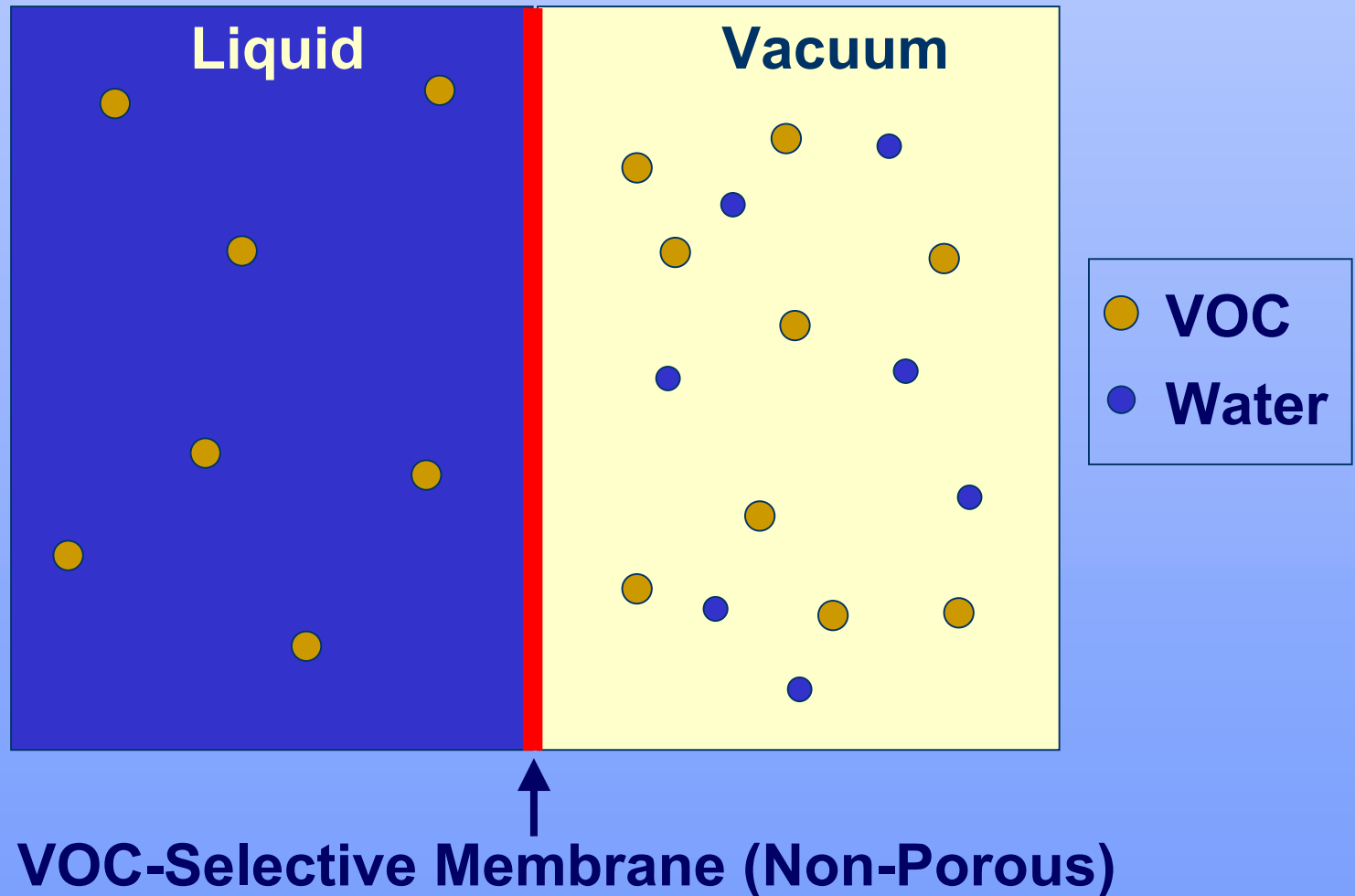
- Contaminants
 - Volatile, semivolatile, non-volatile
- Advantages
 - Applicable to range of contaminants
 - No foaming
- Disadvantages
 - Stability of sorbent
 - Regeneration more complicated

Pervaporation

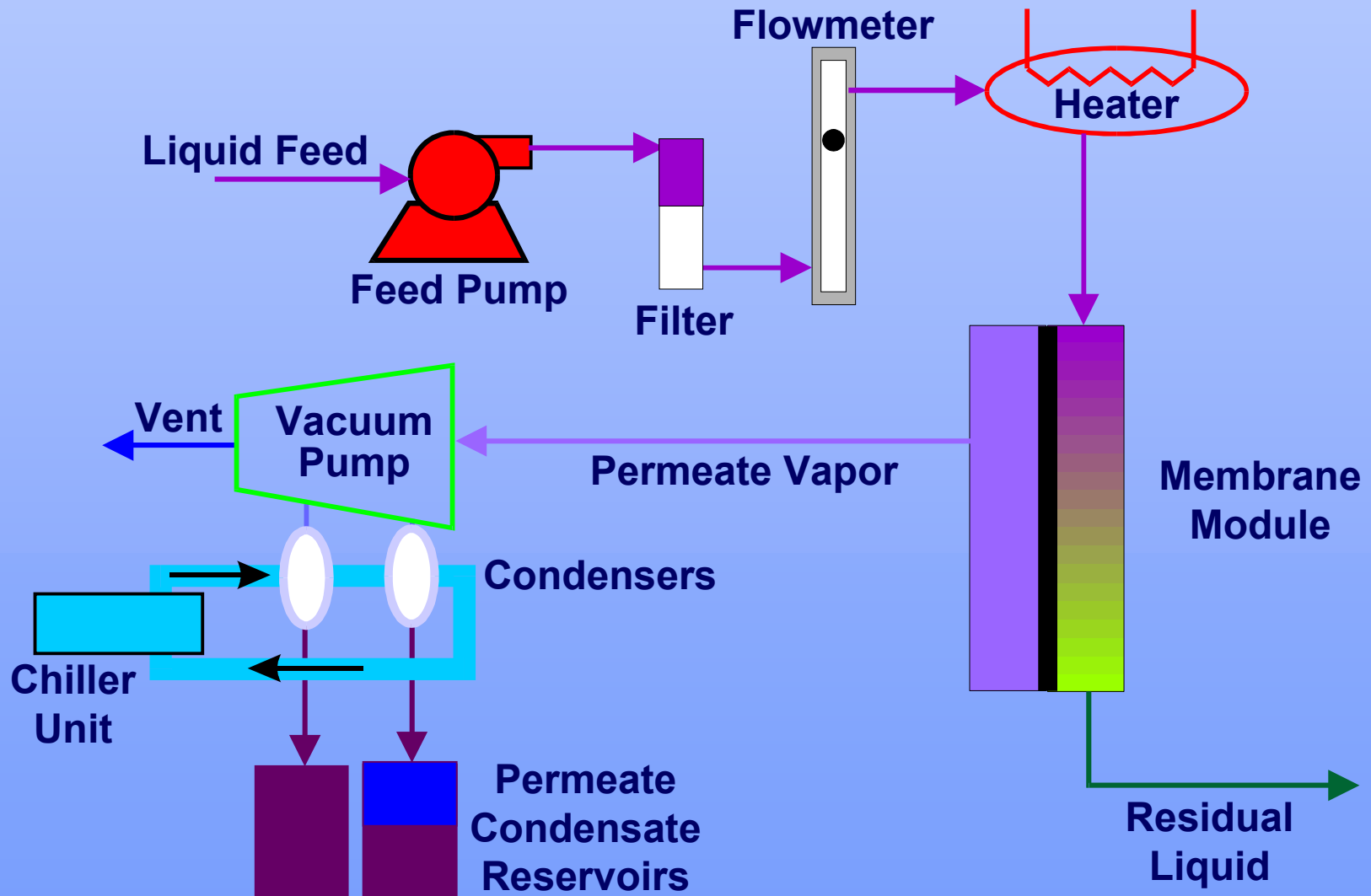
- Contaminants
 - Volatile
- Advantages
 - No foaming
 - Can be used for alcohol recovery
 - Fouling resistant (if designed properly)
- Disadvantages
 - Emerging technology
 - More expensive than air stripping

Pervaporation = Permeation + Evaporation

VOC Removal from Water



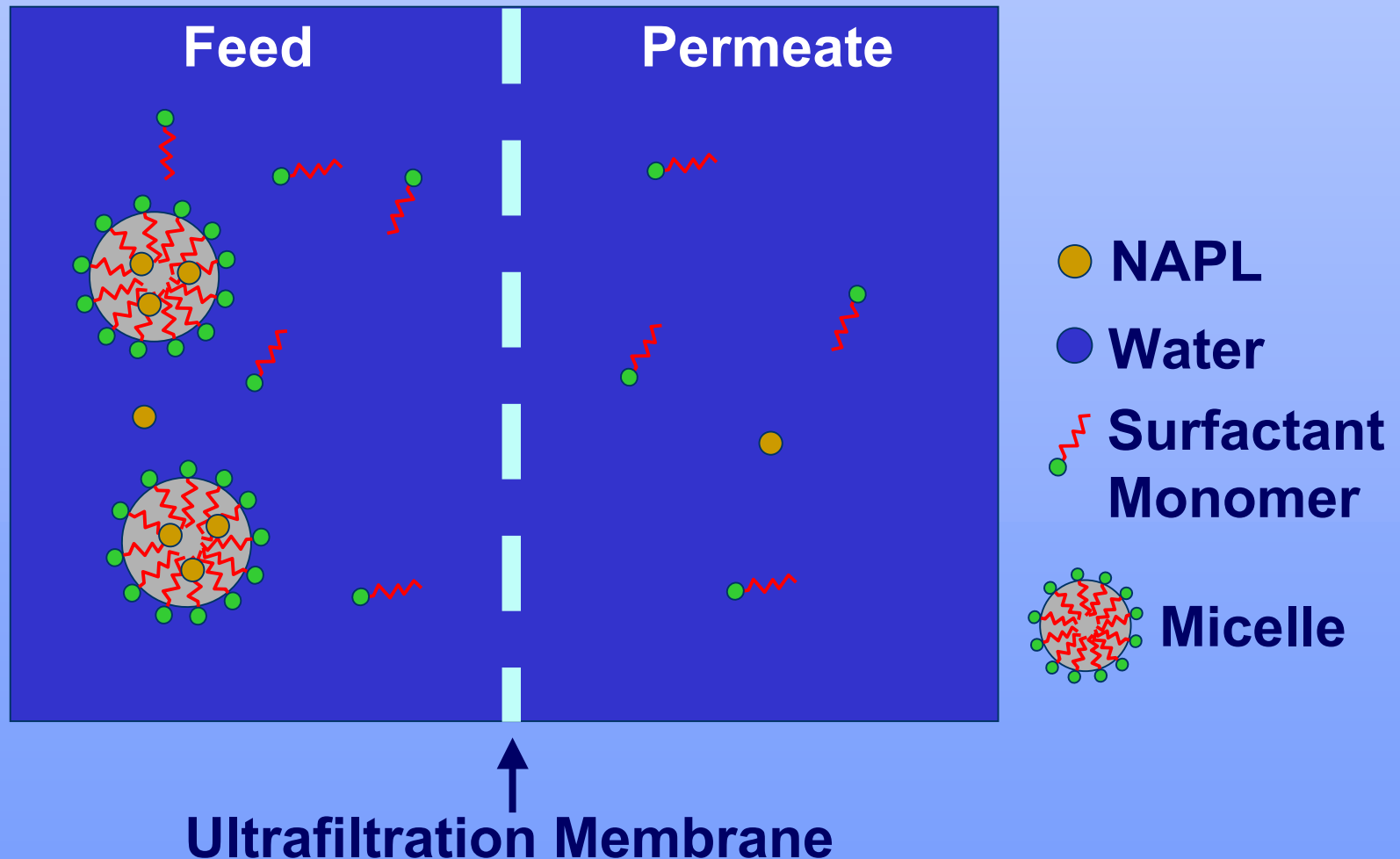
Pervaporation System Components



Surfactant Recovery Technologies

- Micellar-Enhanced Ultrafiltration (MEUF)
- Nanofiltration (NF)
- Foam Fractionation
- Precipitation
- Batch Drying

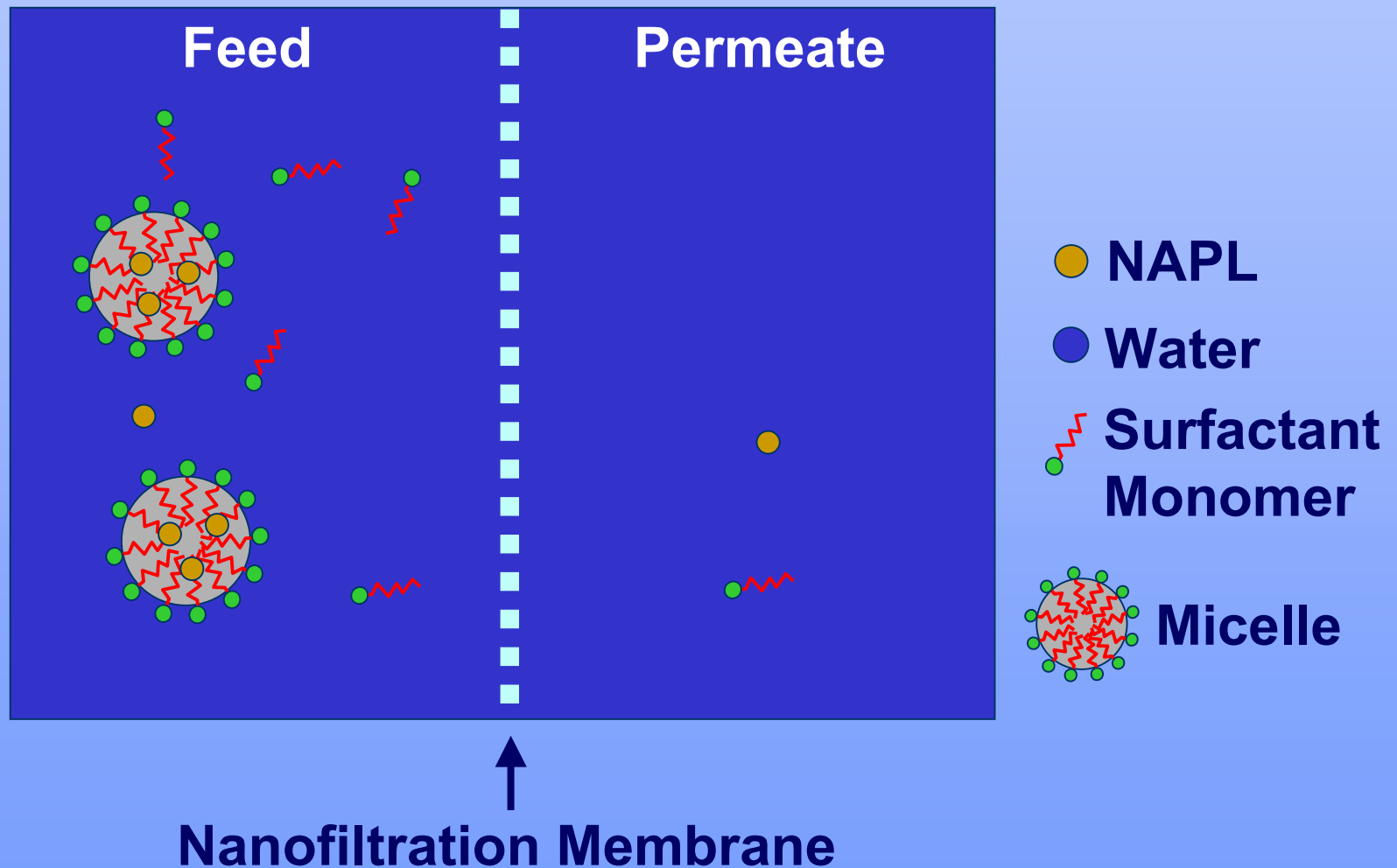
Micellar-Enhanced Ultrafiltration (MEUF)



Micellar-Enhanced Ultrafiltration (MEUF)

- Recovers
 - Surfactant micelles
- Advantages
 - Low cost
 - High % recovery for low CMC surfactant
 - Commercially available
- Disadvantages
 - Surfactant in permeate (further treatment and material loss)
 - Micelle recovery may concentrate contaminants and cations

Nanofiltration (NF)



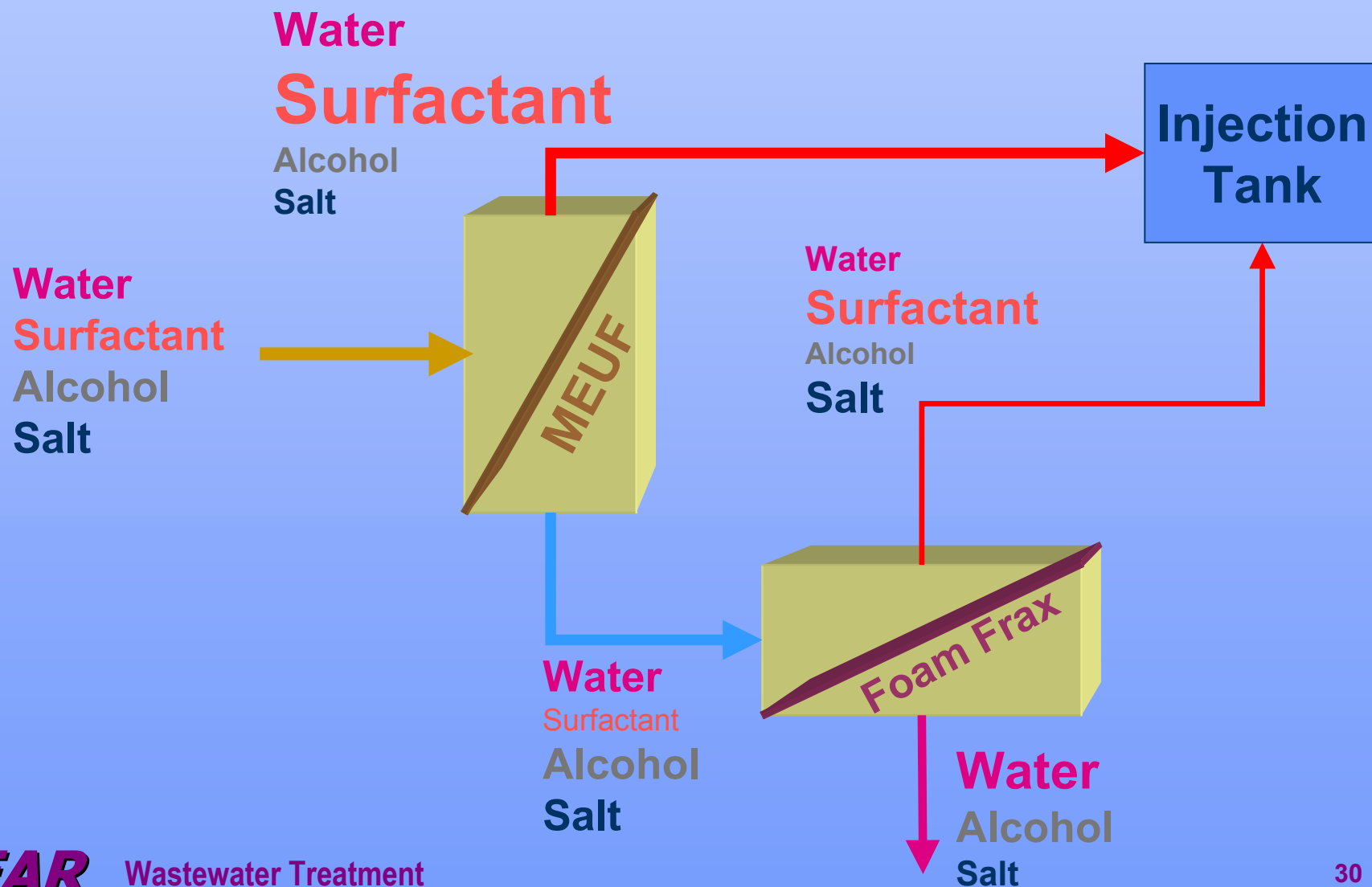
Nanofiltration (NF)

- Recovers
 - Monomers and micelles
- Advantages
 - High % recovery of even monomers
 - Commercially available
- Disadvantages
 - Low membrane flux
 - Higher pressures required
 - Moderate to high cost

Foam Fractionation

- Recovers
 - Surfactant monomer
- Advantages
 - Low cost
 - Can recover monomer
- Disadvantages
 - Not for bulk removal
 - Best for monomer recovery

Hybrid Surfactant Recovery Process



Alcohol Recovery Technologies

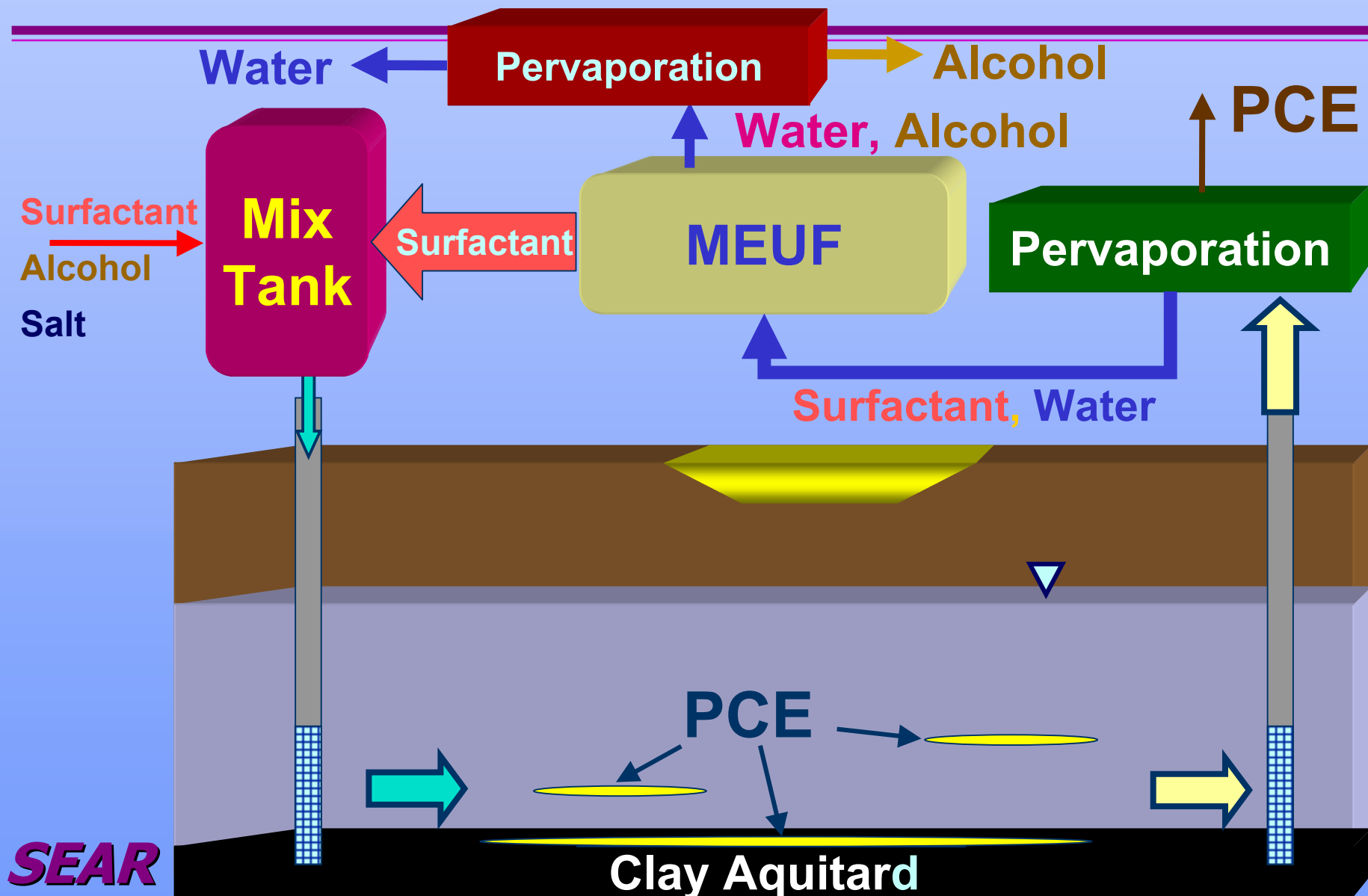
- Pervaporation
- Distillation
- Steam Stripping

ESTCP Field Demonstration

- MCB Camp Lejeune
 - Soil contaminated with dry-cleaning solvent (PCE)
- Objective: To remove PCE from soil using SEAR process and to recycle/reuse the surfactant



ESTCP Field Demonstration



MCB Camp Lejeune Demonstration Participants

- U.S. Navy
- U.S. EPA
- Duke Engineering & Services
- University of Oklahoma
- University of Texas at Austin
- Baker Environmental
- IT Group (OHM, IT Corp.)

U.S. EPA's MCB Camp Lejeune Pervaporation Field Demonstration



U.S. EPA's MCB Camp Lejeune Pervaporation Unit



MCB Camp Lejeune Pervaporation Systems



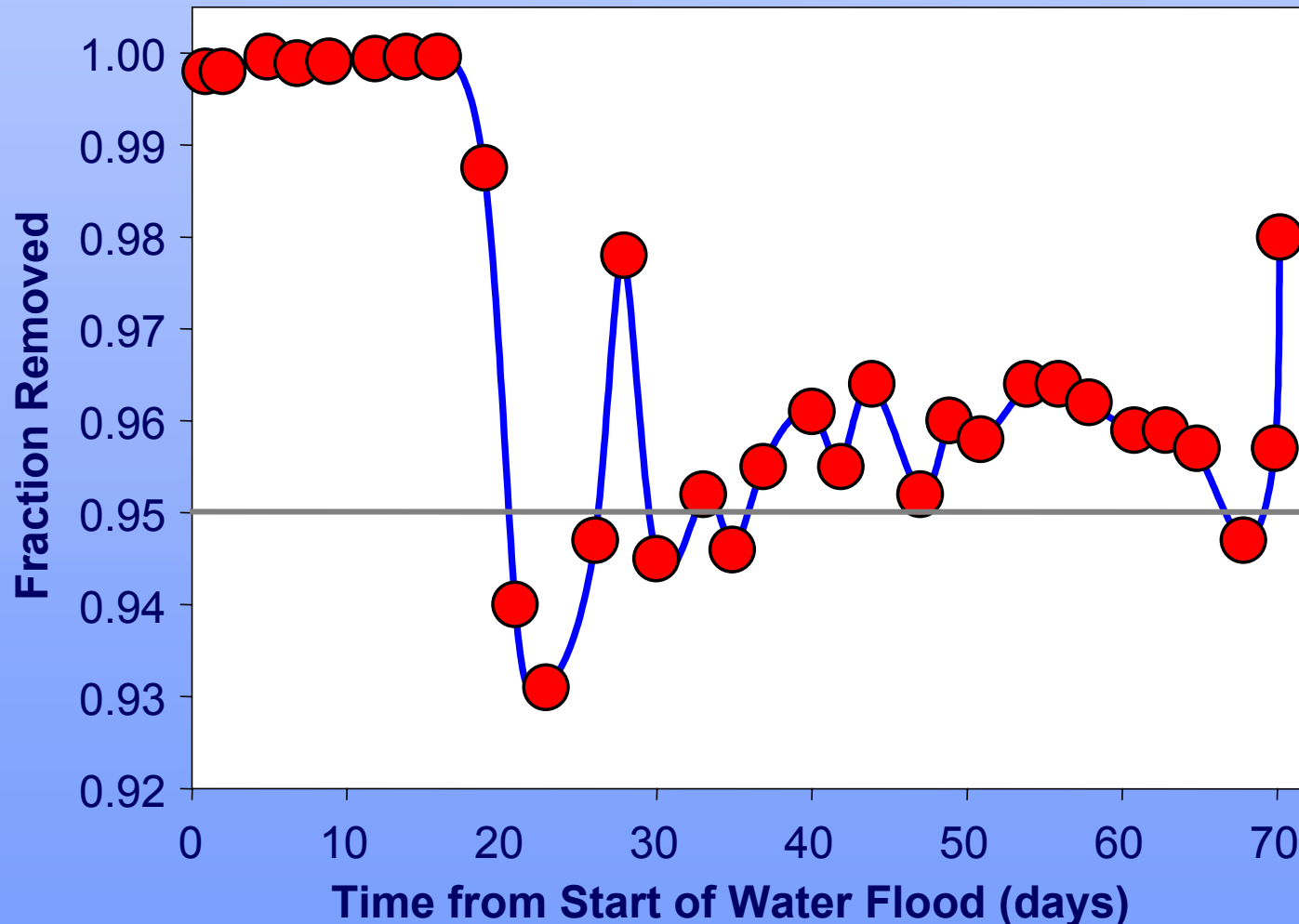
MCB Camp Lejeune Extracted Fluid

- Flow = 1.0 gpm
- Surfactant = 0 to 1.2 wt%
- Isopropyl alcohol = 0 to 4.5 wt%
- PCE = 35 to 1,000 mg/L
- Other VOCs < 5 mg/L
- pH = 4.0 to 4.4
- Ca^{2+} = 250 mg/L
- Fe^{2+} = 15 mg/L

SEAR



PCE Removal by MCB Camp Lejeune Pervaporation Field Unit (95% Removal Objective)



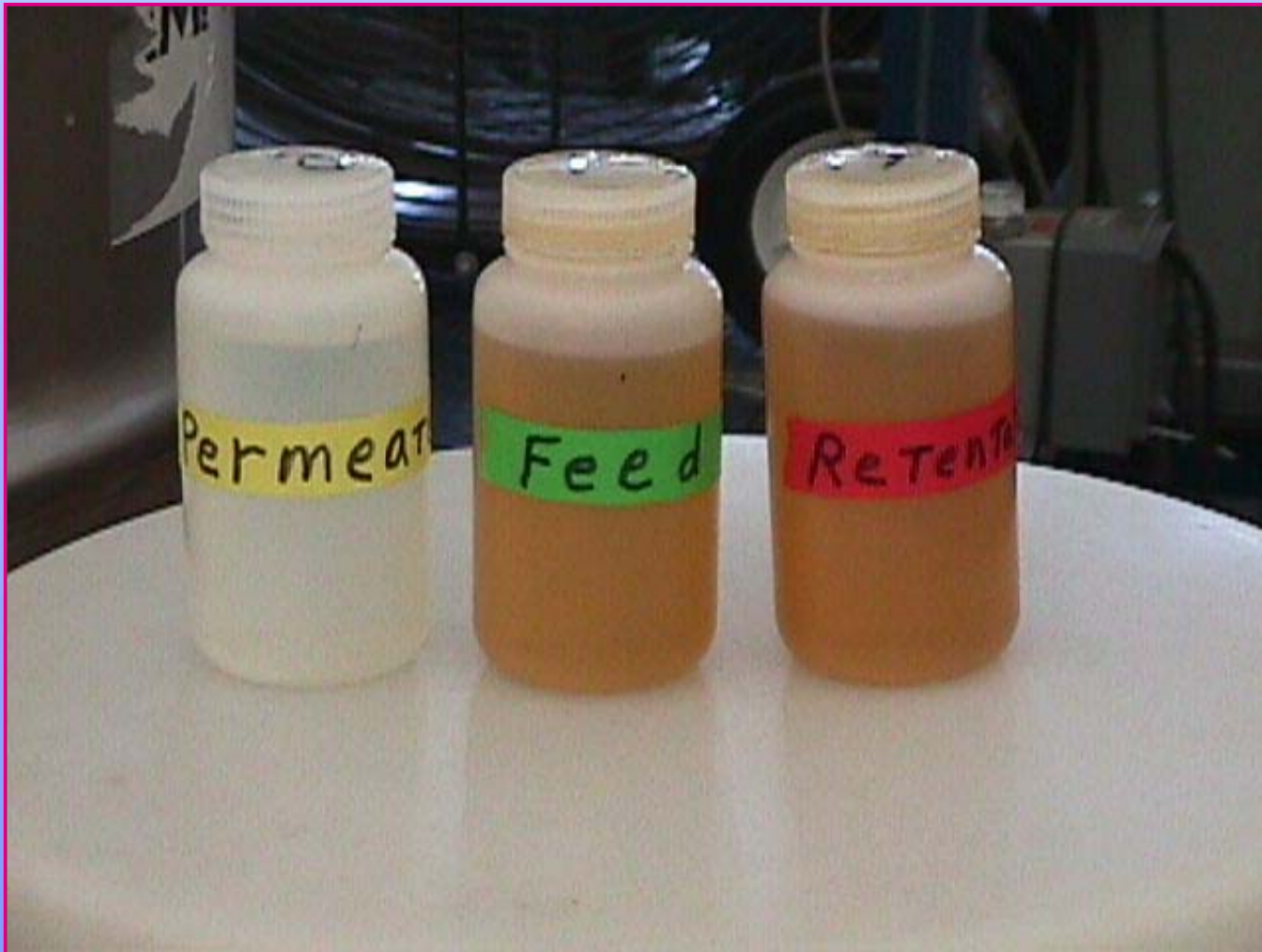
EPA Camp Lejeune Pervaporation Unit: Performance

- PCE Removal
 - Groundwater: 99.94 +/- 0.02 %
 - Surfactant Solution: 95.8 +/- 0.3 %
 - 160 kg (360 lb) PCE removed
- Varsol (Mineral Spirits) Removal
 - Groundwater: < MDL
 - Surfactant Solution: approx. 50%

MEUF Equipment at MCB Camp Lejeune (University of Oklahoma)



MCB Camp Lejeune MEUF Samples



MCB Camp Lejeune MEUF Performance

- 76% surfactant recovery
- 3,800 lb surfactant recovered
- Adversely affected by alcohol

Reinjection Issues

- Reformulation of surfactant
 - Need to maintain desired properties of mixture
- Reinjection of some contaminant
 - No process will remove 100%
- Return of groundwater ions and reaction products to injection wells
 - For example, precipitation of iron caused by oxidation of Fe^{2+}

Competing Scale Issues

High Flow & Short Duration

vs.

Low Flow & Long Duration

- Low cost answer
 - Depends on lease terms/capital costs and operating expenses
 - Also depends on optimum ranges for the technologies

Conclusions

- Wastewater treatment must be considered when designing SEAR process
- Material savings, cost savings, and disposal cost avoidance may motivate treatment decisions
- Technologies are available to perform the necessary separations
- Added technical and logistical issues complicate implementation

Any Questions?

SEAR